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ENVIRONMENTAL
SERVICES

A Division of Cal State Electric Inc.

Ref. 6

COMPLIANCE TEST REPORT

ARCO ALASKA, INC.
P O Box 100360
Anchorage, Alaska 99510

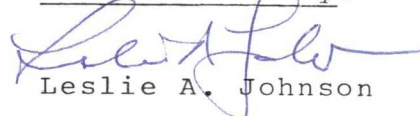
Attention: Jim Ives

Unit: 44.44 MMBTU/hr. Bohn Heater
Tag # G1-14-01

Determination of NOx and O₂
Permit # PSD-X82-01

Tested: September 6, 1985

Units Tested By:


Leslie A. Johnson

Report #: 50-046

Reviewed By:





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ARCO ALASKA, INC.
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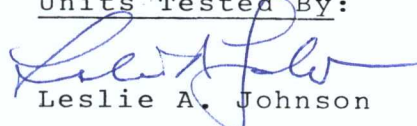
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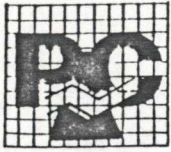
Report #: 50-046

Reviewed By:



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I. INTRODUCTION

INTRODUCTION

On September 6, 1985 Petro-Chem Environmental Services performed emissions source test on the emissions of a 44.44 MMBTU/hr BOHN, Inc. Heater (tag # G1-14-01). The crude heater is located at Arco Alaska, Inc.'s Kuparuk unit topping plant (KUTP).

Emissions of NOx and O2 were monitored at the BOHN heater using the following methods:

<u>Parameter</u>	<u>Method</u>	<u># Runs</u>
NOx	Chemiluminescent NO/NOX Analyzer	3
O2	Fuel Cell O2 Analyzer	3

Unit Operations Cumulation Fuel Meter

Emission test were requested by Arco to document compliance with EPA permit # PSD-X82-01.

An oxygen traverse was performed on a cross sectional grid using EPA method #2 to determine sample points. After confirming that no oxygen stratification existed a single sample point was used for run #2 and #3.

The source tests were conducted by Leslie A. Johnson and Andy Winkler of Petro-Chem Environmental Services. Mr. Jim Ives of Arco Alaska, Inc. was on site to oversee the heaters performance.



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II. SUMMARY OF RESULTS

BOHN HEATER (44.44 MMBTU/hr)

SUMMARY OF RESULTS

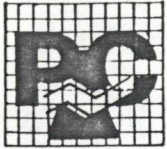
NOx Emissions

<u>NOx, ppm</u>	<u>NOx, ppm @ 3% O₂</u>	<u>lbs/MMBTU</u>	<u>Grams/Joule</u>
68.21	81.80	0.100	4.3 * 10 ⁻⁸

NOx Permit Conditions

(permit #PSD-X82-01)

<u>Unit</u>	<u>Rating</u>	<u>Allowable NOx Emissions</u>	<u>Actual NOx Emissions</u>
Bohn Heater	44.44 MMBTU/hr	0.18 lbs/MMBTU	0.100 lbs/MMBTU



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III. SOURCE OPERATION

BOHN CRUDE HEATER

The crude heater (G1-1401) at the Kuparuk Unit Topping Plant (KUTP) was tested on September 6, 1985 for compliance with the NO_x emissions standards. The heater is utilized to heat crude oil during the production of diesel fuel. The facility can process up to 13000 BOPD and provide a maximum of 3000 barrels of diesel per day.

The Bohn horizontal heater is fired by two John Zink low NO_x Burners (PNCV - Size 70). Each burner has a maximum rating of 22.22 MMBtu/hr. The maximum potential heat release of the heater is 44.44 MMBtu/hr; however, the maximum operating heat release is about 40 MMBtu/hr. The normal operating heat release is 35.56 MMBtu/hr.

JAI2:t1h-20044.1

ARCO ALASKA INC.
 Bohn Heater Tag #G1-14-01
 9/6/85

OPERATING CONDITIONS

<u>Time</u>	<u>Gas Temp F^o</u>	<u>Pres. Psig</u>	<u>Fuel use (MMSCFh)</u>	<u>Cummulative Fuel use (MSCF)</u>
1153	105.4	162.4	31831	331723
1219	105.8	162.4	31704	
1259	104.0	162.5	31601	331757
1423	105.7	162.6	32116	331802
150 min.	1.4.8		31813	79 MSCF

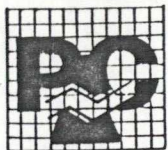
$$79 \text{ MSCF} / 150 \text{ min} * \frac{60 \text{ min}}{1 \text{ hr.}} = 31.6 \text{ MSCF/hr}$$

PROCESS OPERATING CONDITIONS

<u>Unit</u>	<u>Design</u>	<u>Normal Maximum</u>	<u>Actual During Test</u>	<u>% Operation</u>
Bohn Heater	44.44 MMBTU/hr	35.56 MMBTU/hr	37.58 MMBTU/hr	85

$$\text{MMBTU/hr} = \text{MMSCFh} * \frac{\text{BTU}}{\text{SCF}} * \frac{1}{10^6} * \frac{\text{MMBTU}}{10^6 \text{ BTU}} * \frac{10^6 \text{ SCF}}{\text{MSCF}}$$

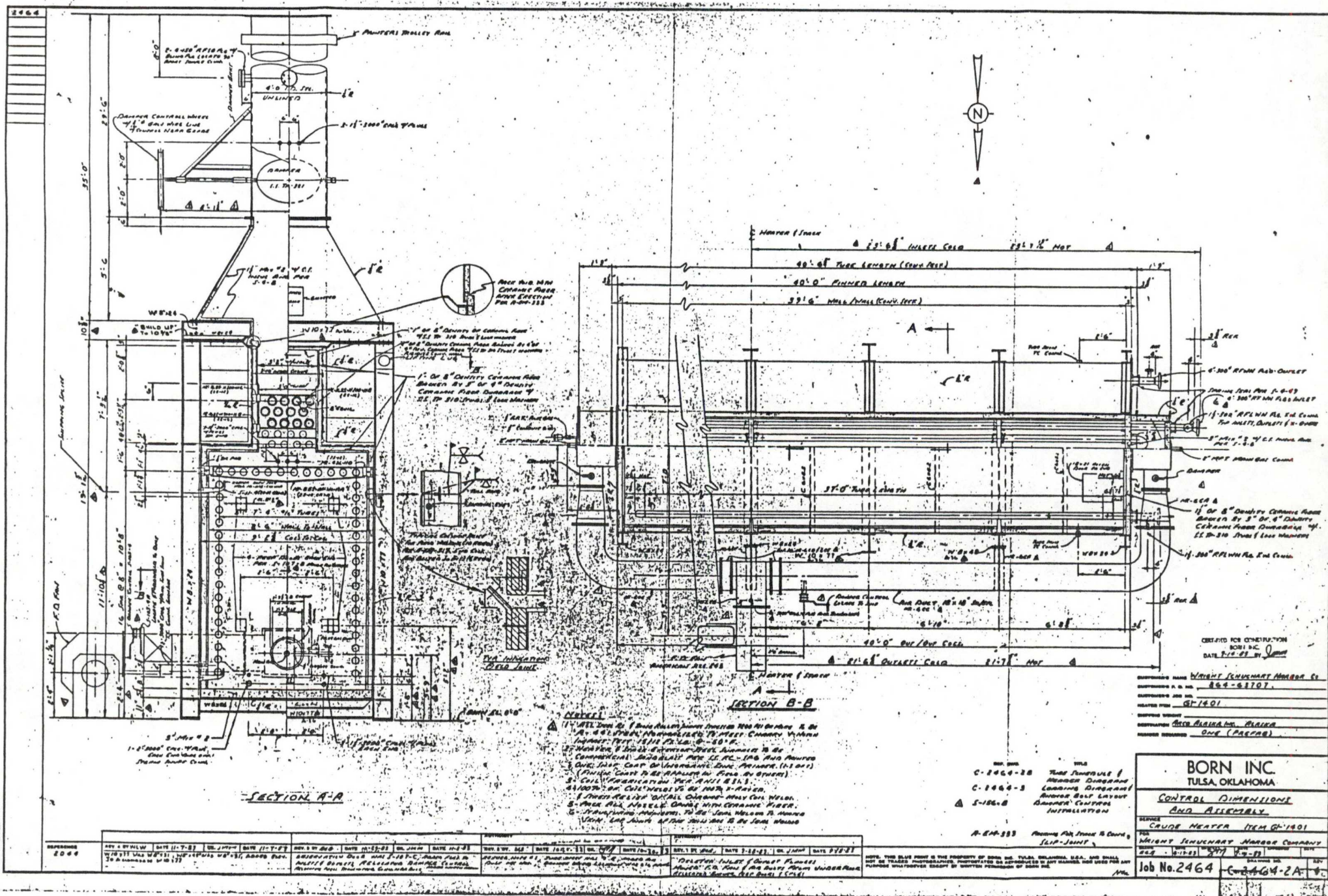
$$\frac{1}{1189.4} \text{ BTU/SCF (see Appendix B)}$$



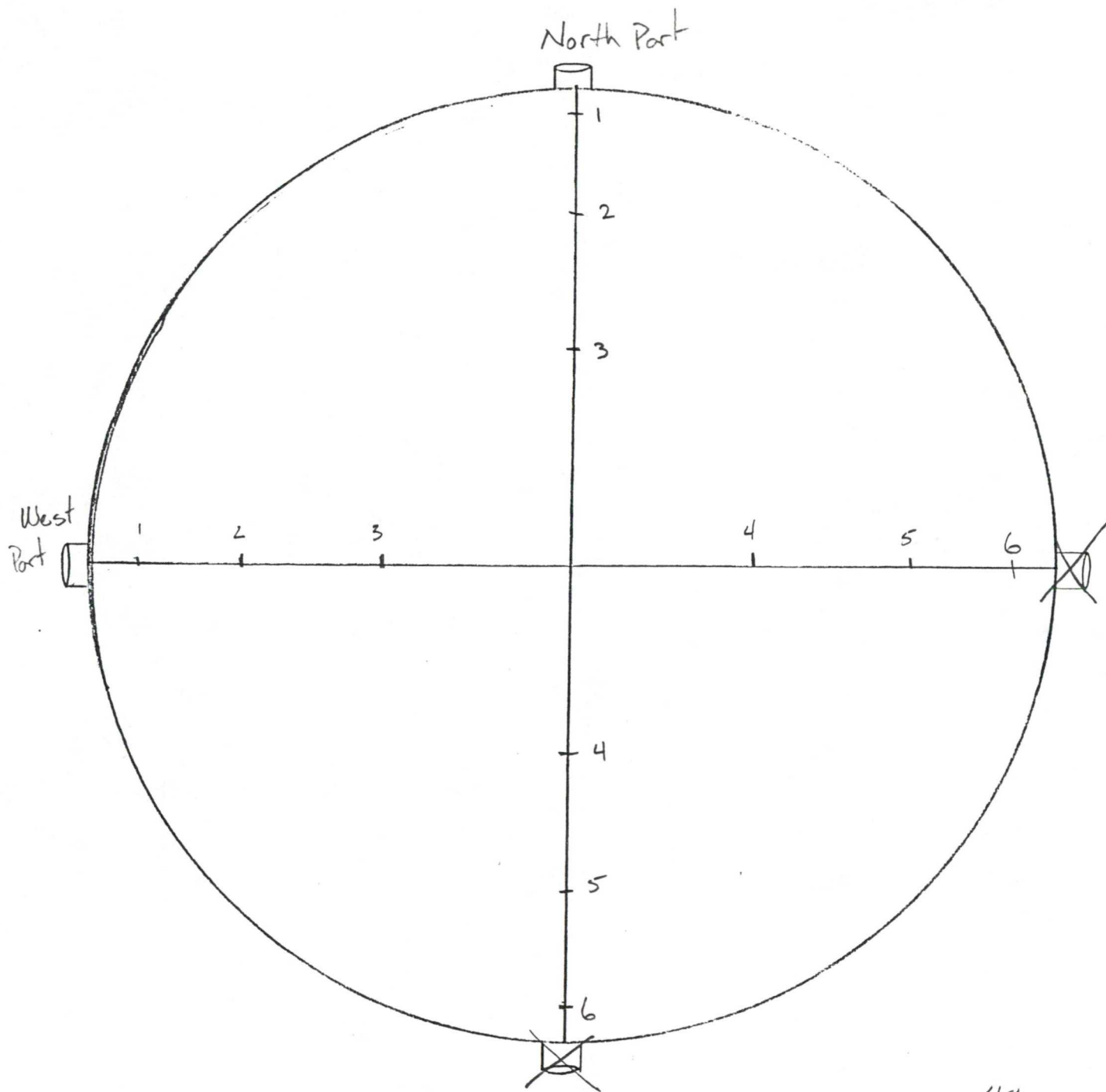
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IV. SAMPLING AND ANALYSIS
PROCEDURES

164



POINT LOCATIONS



Point #	inches from edge
1	2.1
2	7.0
3	14.2
4	33.8
5	41.0
6	45.9
7	
8	
9	
10	

Stack Diameter 48 inches
 Stack Area 12.57 ft²
 Diameters before 2
 Diameters after 5.5
 a disturbance.

CONTINUOUS EMISSION MONITORING SYSTEM (CEMS)

Reference: BAAQMD, Manual of Procedures; ST-13A, St-19A, Jan 1982 State of California, Air Resources Board, Test Methods 1-100, June 1979.

INSTRUMENTATION SUMMARY:

A constant sample of flue gas was extracted, dried, filtered, and delivered to an instrument manifold system for distribution to one or more analyzers. Instrument results are recorded on an analog strip chart recorder. System calibration checks are performed at the beginning and end of each day as well as calibration check at the beginning and end of each test run. Final data reduction includes zero and calibration drift corrections.

SAMPLE CONDITIONING SYSTEM:

Consists of a borosilicate glass tube or 316 grade stainless steel probe fitted with a cindered stainless steel or pyrex glass wool particulate filter. The probe is fitted with a teflon (TFE) sample line which connects to a water condensation system located at the sources. The condensation system consists of two 500 ml stainless steel impingers connected in a series, immersed in an ice bath. The gas is delivered to the instrument trailer with a teflon line (3/8"O.D.) through an in line Balston particulate filter drawn by a teflon coated diaphragm pump. Sample gas is pressurized through a Hankinson gas conditioner which further reduces sample gas moisture insuring against water interference with the instruments. The sample system is leak checked prior to sampling by plugging the end of the sample probe and adjusting the sample pump to it's maximum rate (approximately 22"Hg). The manifold is bypassed and the leak rate monitored through a gas meter or low range flow meter.

MANIFOLD SYSTEM:

Sample gas is delivered to each analyzer through a five (5) way valve and regulated with a needle valve flowmeter. Manifold pressure is controlled by a back pressure regulator which is typically set at three (3) psi. Zero gas (N₂) and calibration gases are delivered to the analyzers using the same five-way valve and flowmeter. All manifold parts are glass, stainless steel, or teflon materials.

CALIBRATION PROCEDURES:

A. System Calibration Procedures:

System calibration checks are performed at the beginning and end of each test day to insure against sample system leaks or contamination. Calibration gas is introduced at the sample probe tip at a normal sample rate and vacuum, the final instrument value must be within $\pm 5\%$ of the calibration gas value.

B. Manifold Calibration:

Instrument calibration checks are performed and adjustments made before and after each test run. Each analyzer is checked with a zero grade nitrogen gas for a zero baseline and then with a calibration gas similar to the expected sample concentration (60-90% of full scale). Calibration gases used in both manifold and system calibrations are with EPA protocol No. 1 gas (traceable to National Bureau of Standards SRM,) or with gases recently analyzed by EPA Reference Methods. All zero and calibration checks are documented and noted on the recorder strip charts.

ANALOG STRIP CHART DATA REDUCTION:

Analog recordings were averaged of time increments as shown on the data pages (typically 5, 10, or 20 minute increments). Data for each increment was recorded at an average percent of full scale. The readings were then compared with the zero and calibration readings for calculation of the average concentration for each time increment. Any deviation of the zero and calibration readings from the start to the end of a test period was corrected by calculating apparent zero and calibration readings for the mid-point of each time increment. The average concentrations were then calculated from the sample readings and the apparent zero and span readings.

2

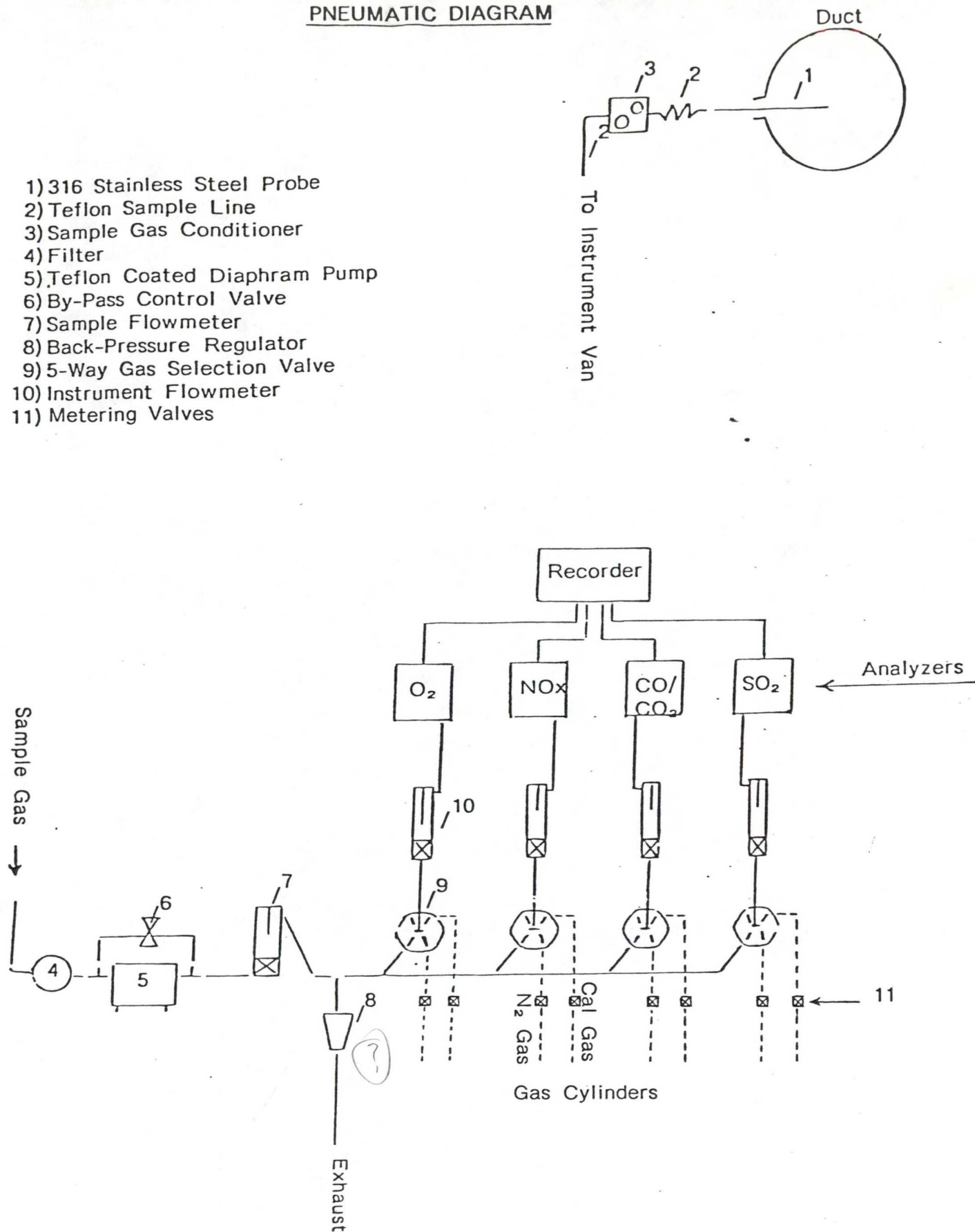
2

ANALOG STRIP CHART DATA REDUCTION:

Analog recordings were averaged of time increments as shown on the data pages (typically 5, 10, or 20 minute increments). Data for each increment was recorded at an average percent of full scale. The readings were then compared with the zero and calibration readings for calculation of the average concentration for each time increment. Any deviation of the zero and calibration readings from the start to the end of a test period was corrected by calculating apparent zero and calibration readings for the mid-point or each time increment. The average concentrations were then calculated from the sample readings and the apparent zero and span readings.

PNEUMATIC DIAGRAM

- 1) 316 Stainless Steel Probe
- 2) Teflon Sample Line
- 3) Sample Gas Conditioner
- 4) Filter
- 5) Teflon Coated Diaphragm Pump
- 6) By-Pass Control Valve
- 7) Sample Flowmeter
- 8) Back-Pressure Regulator
- 9) 5-Way Gas Selection Valve
- 10) Instrument Flowmeter
- 11) Metering Valves



RESPONSE TIME

Date of Test: September 2, 1985

Analyzer Type: NO/NO_x Thermo Electron Analyzer

Span Gas Concentration: 100 (ppm or %)

Zero Gas Source: Ambient Air

Upscale:

- 1) 45 seconds
- 2) 50 seconds
- 3) 50 seconds

Average upscale response 48.3 seconds.

Downscale:

- 1) 45 seconds
- 2) 45 seconds
- 3) 40 seconds

Average downscale response 43.3 seconds.

Systems response time 60 seconds.

This is response time
check, but it's
not clear what
is being shown

BW 12/13

22

20

30

40

50

60

70

80

90

21

58/7/6
01/10/6

RECEIVED 20 11/10/6
10/10/6

20

WIL-
FISHERY
XON
1-11
10/10/6
10/10/6

20

30

40

50

60

70

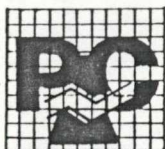
80

90

19

L I N E I S

18



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V. APPENDIXES

ARCO ALASKA, INC.
Bohn Heater

NOx RESULTS

<u>Run #</u>	<u>Time</u>	<u>% O₂</u>	<u>NOx ppm</u>	<u>NOx ppm @ 3% O₂</u>	<u>NOx lbs/MMBTU</u>
1	1155-1255	5.94	64.71	77.44	0.095
2	1300-1340	6.01	69.96	84.07	0.103
3	1345-1425	<u>5.97</u>	<u>69.96</u>	<u>83.88</u>	<u>0.103</u>
Average		5.97	68.21	81.80	0.100 ✓

$$\text{lbs/MMBTU} = \text{ppm} * \frac{20.9}{20.9 - \%O_2} * \text{MW} * \text{F factor} * 2.635 * 10^{-9}$$

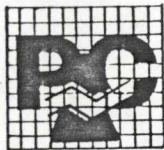
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ARCO ALASKA, INC.
Bohn Heater

NOx RESULTS

<u>Run #</u>	<u>Time</u>	<u>% O₂</u>	<u>NOx ppm</u>	<u>NOx ppm @ 3% O₂</u>	<u>NOx lbs/MMBTU</u>
1	1155-1255	5.94	64.71	77.44	0.095
2	1300-1340	6.01	69.96	84.07	0.103
3	1345-1425	<u>5.97</u>	<u>69.96</u>	<u>83.88</u>	<u>0.103</u>
Average		5.97	68.21	81.80	0.100 ✓

$$\text{lbs/MMBTU} = \text{ppm} * \frac{20.9}{20.9 - \%O_2} * \text{MW} * \text{F factor} * 2.635 * 10^{-9}$$



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APPENDIX A

NOx and O₂ RESULTS

COMPANY:ARCO ALASKA, INC

DATE: 9-6-85

UNIT: KUPARUK BOHN Heater Tag #G1-14-01

RUN# 1
NOX/O2 DATA

TIME INTERVAL		CONCENTRATION;FULL SCALE CONCENTRATION; CORRECTED			
BEGIN	END	O2;fs	NOx;fs	O2;%	NOx;ppm
1	1155	1200	34 23.3	5.90	66.46
2	1200	1205	34 23.3	5.90	66.46
3	1205	1210	34 23.2	5.90	65.96
4	1210	1215	33.5 23	5.78	64.96
5	1215	1220	33.5 23	5.78	64.96
6	1220	1225	33.5 23	5.78	64.96
7	1225	1230	34 23	5.90	64.96
8	1230	1235	34 23	5.90	64.96
9	1235	1240	34.5 23	6.02	64.96
10	1240	1245	35 22.6	6.15	62.96
11	1245	1250	35 22.6	6.15	62.96
12	1250	1255	35 22.4	6.15	61.96

1155	1255	33.75	23.13	5.94	64.71
Averages					

	O2	NOX
INITIAL ZERO(%fs)	10	10
INITIAL SPAN(%fs)	95	30
FINAL ZERO (%fs)	10	10
FINAL SPAN (%fs)	95	30
% ZERO DRIFT:	0.00	0.00
% SPAN DRIFT:	0.00	0.00
CAL GAS(ppm or %)	20.9	99.94
RANGE (ppm or%)	25	500

RUN 1			
NOx	%O2	NOx,ppm	NOx ppm@ 3% O2
	5.94	64.71	77.44

COMPANY: ARCO ALASKA, INC
 DATE: 9-6-85
 UNIT: KUPARUK BOHN Heater Tag #G1-14-01

RUN# 2
 NOX/O2 DATA

TIME INTERVAL		CONCENTRATION; FULL SCALE		CONCENTRATION; CORRECTED	
BEGIN	END	O2; fs	NOx; fs	O2; %	NOx; ppm
1	1300	1305	34.5	24	6.01 69.96
2	1305	1310	34.5	24	6.03 69.96
3	1310	1315	34.5	24	6.05 69.96
4	1315	1320	34.5	24	6.07 69.96
5	1320	1325	34	24	5.96 69.96
6	1325	1330	33.7	24	5.91 69.96
7	1330	1335	34	24	6.00 69.96
8	1335	1340	34	24	6.02 69.96
1300 1340		34.28	24.00	6.01	69.96
Averages					

	O2	NOX
INITIAL ZERO(%fs)	10	10
INITIAL SPAN(%fs)	95.5	30
FINAL ZERO (%fs)	10	10
FINAL SPAN (%fs)	98	30
% ZERO DRIFT:	0.00	0.00
% SPAN DRIFT:	2.62	0.00
CAL GAS(ppm or %)	20.9	99.94
RANGE (ppm or%)	25	500

RUN 2			
NOx	%O2	NOx, ppm	NOx ppm @ 3% O2
	6.01	69.96	84.07

COMPANY:ARCO ALASKA, INC

DATE: 9-6-85

UNIT: KUPARUK BOHN Heater Tag #G1-14-01

RUN# 3

NOX/O2 DATA

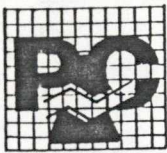
TIME INTERVAL		CONCENTRATION; FULL SCALE		CONCENTRATION; CORRECTED	
BEGIN	END	O2; fs	NOx; fs	O2; %	NOx; ppm
1	1345	1350	34	24	5.97 69.96
2	1350	1355	34	24	5.97 69.96
3	1355	1400	34	24	5.97 69.96
4	1400	1405	34	24	5.97 69.96
5	1405	1410	34	24	5.97 69.96
6	1410	1415	34	24	5.97 69.96
7	1415	1420	34	24	5.97 69.96
8	1420	1425	34	24	5.97 69.96

1345	1425	34.00	24.00	5.97	69.96
Averages					

	O2	NOX
INITIAL ZERO(%fs)	10	10
INITIAL SPAN(%fs)	94	30
FINAL ZERO (%fs)	10	10
FINAL SPAN (%fs)	94	30
% ZERO DRIFT:	0.00	0.00
% SPAN DRIFT:	0.00	0.00
CAL GAS(ppm or %)	20.9	99.94
RANGE (ppm or%)	25	500

RUN 3

	%O2	NOx, ppm	NOx ppm @ 3% O2
NOx	5.97	69.96	83.88



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APPENDIX B

FUEL ANALYSIS & F FACTOR

CLIENT:ARCO Alaska
UNIT:KUTP Bohn Crude Heater
REPORT#:50-022
DATE:9-06-85

Expansion Factor
x Mole % = Exhaust

EPA "F" FACTOR FOR FUEL GAS

FUEL COMPONENT	C	H	EXPANSION FACTOR	COMPONENT MOLE %	EXHAUST DSCF (0)/ SCF FUEL
METHANE	1	4	8.57	84.14	7.21
ETHANE	2	6	15.25	7.57	1.15
PROPANE	3	8	21.92	4.31	0.94
(ISO- BUTANE)	4	10	28.6	0.65	0.19
NORM- BUTANE	4	10	28.6	1.32	0.38
(ISO- PENTANE)	5	12	35.28	0.40	0.14
NORM- PENTANE	5	12	35.28	.27	0.10
HEXANE +	6	14	41.95	0.13	0.05
AIR (N2+O2)	-	-	1	0.32	.0032
CO2	-	-	1	0.89	.0089
H2S	-	2	1	0	0
TOTAL				100	10.18

Where does .27
come from? endothermic?

APP B

10.17	DSCF EXHAUST PER SCF OF FUEL GAS AT ZERO % OXYGEN
1077.3	NET BTU/SCF OF FUEL GAS
1189.4	GROSS BTU/SCF OF FUEL GAS
8552.54	DSCF/MMBTU (EPA "F" FACTOR @ 60 °F & ZERO % OXYGEN)
8682.78	DSCF/MMBTU (EPA "F" FACTOR @ 68 °F & ZERO % OXYGEN)

CLIENT:ARCO Alaska
 UNIT:KUTP Bohn Crude Heater
 REPORT#:50-022
 DATE:9-06-85

EPA "F" FACTOR FOR FUEL GAS

FUEL COMPONENT	C	H	EXPANSION FACTOR	COMPONENT MOLE %	EXHAUST DSCF (0)/ SCF FUEL
METHANE	1	4	8.57	84.14	7.21
ETHANE	2	6	15.25	7.57	1.15
PROPANE	3	8	21.92	4.31	0.94
(ISO- BUTANE)	4	10	28.6	0.65	0.19
NORM- BUTANE	4	10	28.6	1.32	0.38
(ISO- PENTANE)	5	12	35.28	0.40	0.14
NORM- PENTANE	5	12	35.28	.27	0.10
HEXANE +	6	14	41.95	0.13	0.05
AIR (N2+O2)	-	-	1	0.32	.0032
CO2	-	-	1	0.89	.0089
H2S	-	2	1	0	0
TOTAL				100	10.18

10.17	DSCF EXHAUST PER SCF OF FUEL GAS AT ZERO % OXYGEN
1077.3	NET BTU/SCF OF FUEL GAS
1189.4	GROSS BTU/SCF OF FUEL GAS
8552.54	DSCF/MMBTU (EPA "F" FACTOR @ 60 °F & ZERO % OXYGEN)
8682.78	DSCF/MMBTU (EPA "F" FACTOR @ 68 °F & ZERO % OXYGEN)

ARCO ALASKA, INC.
PRUDHOE BAY CENTRAL LABORATORY
ANALYSIS REPORT

SAMPLE# 025101 ARCHIVE# 0696011ZA

19 SEP 1985

SEP 3

location, KUPARUK LPH#1 company, ARCO
sample month, day, year, hour, sample point description
9 6 1985 1055 KUTP FUEL GAS
sample description
FUEL GAS
temp, sample PSIG, line PSIG, meter#
105.5 ** 163 **
requestor
M. SCHAUER

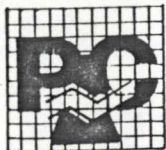
PROPERTY	VALUE	
SAMPLE TIME	1055	HOURS
TEMPERATURE	105.5	DEG. F
LINE PRESSURE	163	PSIG
NITROGEN	.32	MOL %
METHANE	84.14	MOL %
CARBON DIOXIDE	.89	MOL %
ETHANE	7.57	MOL %
PROPANE	4.31	MOL %
ISOBUTANE	.65	MOL %
N-BUTANE	1.32	MOL %
ISOPENTANE	.4	MOL %
N-PENTANE	.	MOL %
C6+	.	MOL %
HYDROGEN SULFIDE	0	MOL %
GROSS DRY (IDEAL GAS)	1172.4	BTU/CF
NET (IDEAL GAS)	1177.3	BTU/CF
GROSS SATURATED IDEAL	1171.5	BTU/CF
SP GRAVITY (CALC.)	.687	
SP GRAVITY (MEAS.)	***	

COMMENTS:

.....

COMPLETED BY:.....

REVIEWED BY:.....



PETRO
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APPENDIX C
RAW FIELD DATA

Bohn Heater

(Arco tag #gl-14-01)

9/6/85

44.44 MMBTU/hr output

located at Kuparuk unit topping plant.

Two 4' ports on a horizontal plane 90° apart approximately 5.5 diameters downstream and two (2) diameters upstream from a disturbance in the flow.

Stack dia: 4 ft.

Stack area: 12.57 ft.²

Static pressure -0.14

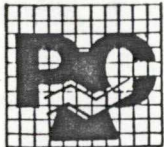
<u>pt #</u>	<u>inches from edge:</u>	<u>Td</u>
1	2.1	794°F
2	7.0	789°F
3	14.2	792°F
4	33.8	
5	41.0	
6	45.9	

Present:

Jim Ives - Arco

Testers:

Leslie A. Johnson - PCES
Andy Winkler - PCES



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APPENDIX D

QUALITY ASSURANCE



Scott Specialty Gases

a division of
Scott Environmental Technology, Inc.

PLUMSTEADVILLE, PA. 18949

PHONE: 215-766-8861

TWX: 510-665-9344

PETRO CHEM ENV.
ATTN: JIM MARCHESINI
3207 ANTONINO
BAKERSFIELD, CA 93308

Date Shipped 9/27/85

Our Project No: 330404

Your P.O. No: VERBAL

Page 1 of 2

CERTIFICATE OF ANALYSIS - EPA PROTOCOL GASES*

(Concentrations are in mole % or ppm)

Cylinder Number AAL-14186 Certified Accuracy ±1 % NBS Traceable Analysis Dates: First 9/18/85 Last 9/26/85

COMPONENTS	CERTIFIED CONC	EXPIRATION DATE	ANALYTICAL PRINCIPLE	PRIMARY STANDARD NBS/SRM's	REPLICATE CONCENTRATIONS	
					FIRST	SECOND
SULFUR DIOXIDE	22.66 ppm	3/26/86	ELECTROCHEMICAL	1694/1693	22.65 ppm	22.66 ppm
NITROGEN	BALANCE				22.62 ppm	22.66 ppm
					22.56 ppm	22.68 ppm

Cylinder Number AAL-14186 Certified Accuracy ±1 % NBS Traceable Analysis Dates: First 9/16/85 Last 9/23/85

COMPONENTS	CERTIFIED CONC	EXPIRATION DATE	ANALYTICAL PRINCIPLE	PRIMARY STANDARD NBS/SRM's	REPLICATE CONCENTRATIONS	
					FIRST	SECOND
NITRIC OXIDE	99.94 ppm	3/23/86	CHEMILUMINESCENCE	1684/1683	99.92 ppm	99.85 ppm
NITROGEN	BALANCE				99.42 ppm	99.99 ppm
					99.69 ppm	99.99 ppm

*We hereby certify the cylinder gas has been analyzed according to EPA Protocol No:

Analyst GREG WIMMER

Approved By FRANCIS E. NEWELL

The only liability of this Company for gas which fails to comply with this analysis shall be replacement thereof by the Company without extra cost.

CERTIFIED REFERENCE MATERIALS ☐ EPA PROTOCOL GASES ☐ ACUBLEND® ☐ CALIBRATION & SPECIALTY GAS MIXTURES
PURE GASES ☐ ACCESSORY PRODUCTS ☐ CUSTOM ANALYTICAL SERVICES



Scott Specialty Gases

a division of

Scott Environmental Technology, Inc.

PLUMSTEADVILLE, PA. 18949

PHONE: 215-766-8861

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PETRO CHEM

ATTN: JIM MARCHESINI

Date Shipped 9/27/85

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Your P.O. No: VERBAL

Page 2 of 2

CERTIFICATE OF ANALYSIS - EPA PROTOCOL GASES*

(Concentrations are in mole % or ppm)

AAL-14186

Cylinder Number _____ Certified Accuracy ±1 % NBS Traceable

Analysis Dates: First 9/18/85 Last 9/26/85

COMPONENTS	CERTIFIED CONC	EXPIRATION DATE	ANALYTICAL PRINCIPLE	PRIMARY STANDARD NBS/SRM's	REPLICATE CONCENTRATIONS	
					FIRST	SECOND
CARBON MONOXIDE	25.13 ppm	3/26/86	NDIR	1679c/2614	25.17 ppm	25.16 ppm
NITROGEN	BALANCE				25.04 ppm	25.12 ppm
					25.09 ppm	25.11 ppm

Cylinder Number _____ Certified Accuracy _____ % NBS Traceable

Analysis Dates: First _____ Last _____

COMPONENTS	CERTIFIED CONC	EXPIRATION DATE	ANALYTICAL PRINCIPLE	PRIMARY STANDARD NBS/SRM's	REPLICATE CONCENTRATIONS	
					FIRST	SECOND

*We hereby certify the cylinder gas has been analyzed according to EPA Protocol No:

Analyst

GREG WIMMER

Approved By

FRANCIS E. NEVILL

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TROY, MICHIGAN / SAN BERNARDINO, CALIFORNIA / HOUSTON, TEXAS

PETRO-CHEM ENVIRONMENTAL SERVICES

INSTRUMENT LINEARITY TEST

DATE: October 9, 1985

CALIBRATION GASES: EPA Protocol 1

OPERATOR: A. Winkler

HIGH CONCENTRATION:

MANUFACTURER: Thermo-Electron

LOW CONCENTRATION: 64 ppm CO

ANALYZER: CO

DILUTION GAS: N₂ (zero grade)

MODEL: 48

INSTRUMENT RANGE: 0 - 100 ppm

SERIAL #: 48-17394-169

INSTRUMENT MODE SETTING: 0 - 30 sec.
time constant

GAS BLENDER SETTINGS:

INSTRUMENT RESULTS

<u>Blend Gas (L/Min)</u>	<u>Dilution Gas (L/Min)</u>	<u>Blended Value</u>	<u>Instrument Value</u>	<u>% Deviation</u>
0.0	2.0	0	0	0.0
2.0	0.0	64	64	0.0
1.5	0.5	48	47	0.2
1.0	1.0	32	32	0.0
0.5	1.5	16	16	0.0
0.0	2.0	0	0	0.0
2.0	0.0	64	64	0.0

PETRO-CHEM ENVIRONMENTAL SERVICES

INSTRUMENT LINEARITY TEST

DATE: October 9, 1985

OPERATOR: A. Winkler

MANUFACTURER: Teledyne

ANALYZER: Oxygen

MODEL: 320 AX

SERIAL #: 90840

CALIBRATION GASES: EPA Protocol 1

HIGH CONCENTRATION:

LOW CONCENTRATION: 21 (ambient)

DILUTION GAS: N₂ (zero grade)

INSTRUMENT RANGE: 0 - 25%

INSTRUMENT MODE SETTING:

GAS BLENDER SETTINGS:

INSTRUMENT RESULTS

<u>Blend Gas (L/Min)</u>	<u>Dilution Gas (L/Min)</u>	<u>Blended Value</u>	<u>Instrument Value</u>	<u>% Deviation</u>
0.0	2.0	0	0	0.0
2.0	0.0	21	21	0.0
1.5	0.5	15.7	15.5	1.0
1.0	1.0	10.5	10.7	0.8
0.5	1.5	5.2	5.2	0.0
0.0	2.0	0	0	0.0
2.0	0.0	21	21	0.0

PETRO-CHEM ENVIRONMENTAL SERVICES

INSTRUMENT LINEARITY TEST

DATE: October 9, 1985

CALIBRATION GASES: EPA Protocol 1

OPERATOR: A. Winkler

HIGH CONCENTRATION:

MANUFACTURER: Thermo-Electron

LOW CONCENTRATION: 277 ppm NOx

ANALYZER: NOx

DILUTION GAS: N₂ (zero grade)

MODEL: 10

INSTRUMENT RANGE: 0 - 500 ppm

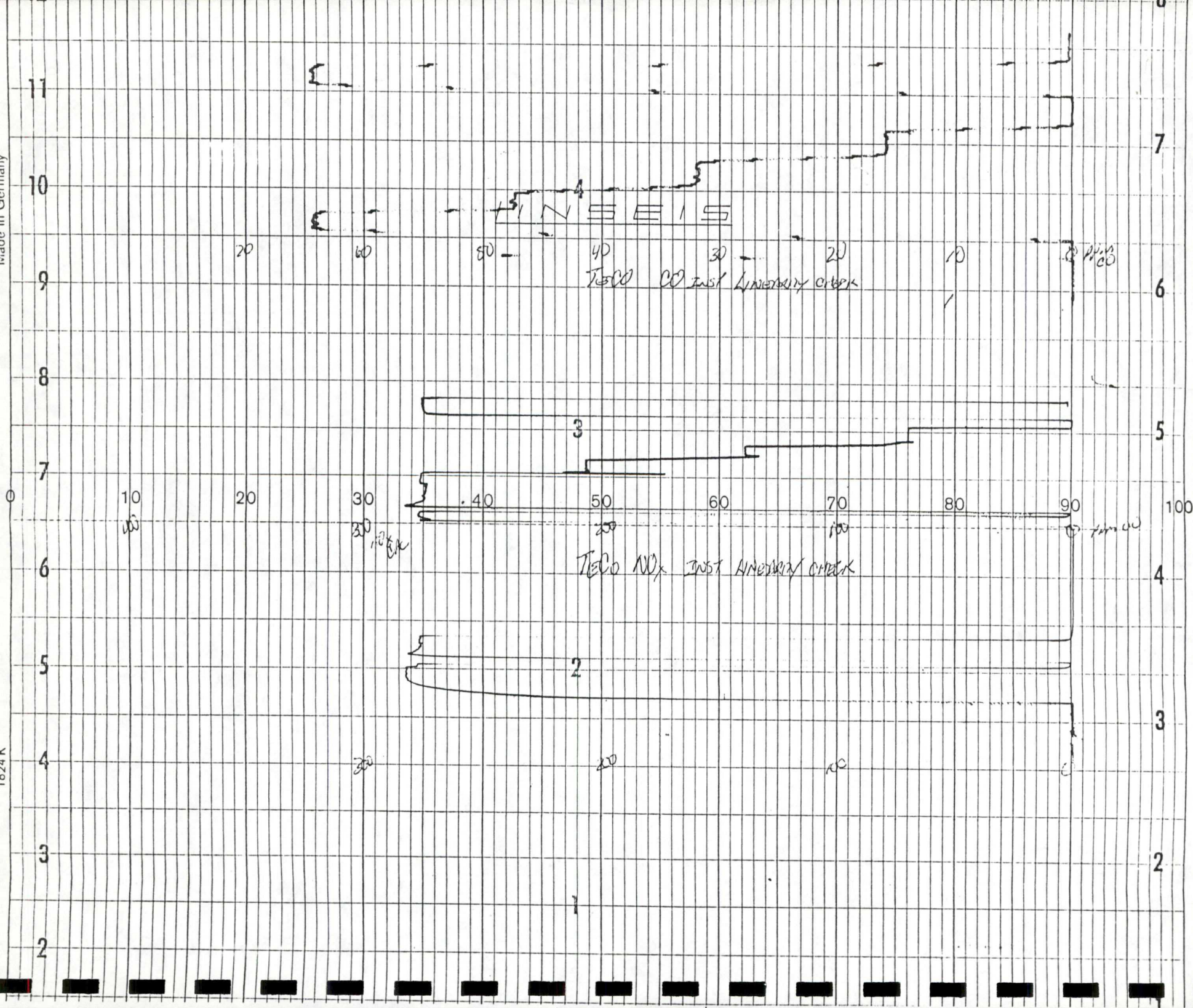
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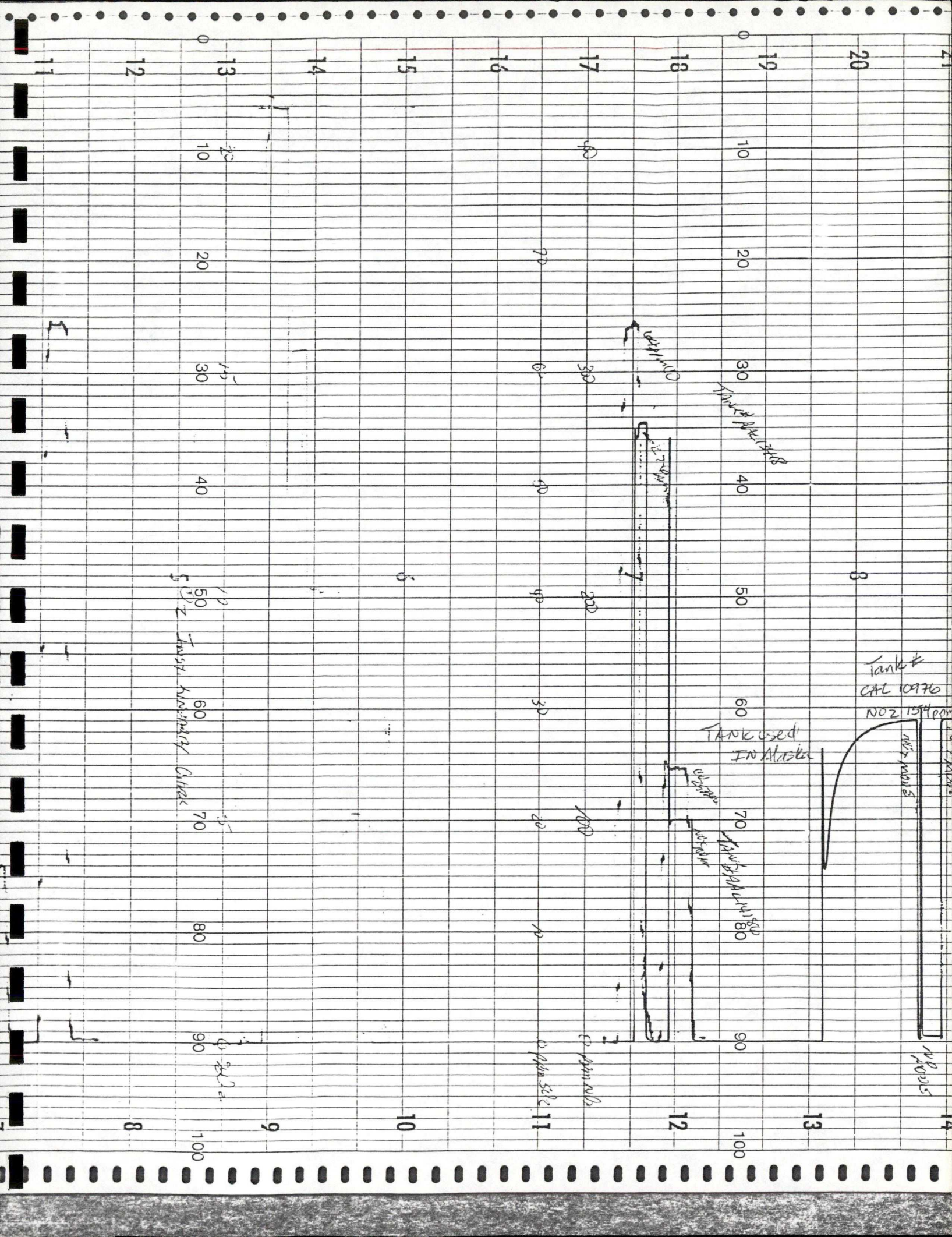
INSTRUMENT MODE SETTING: Converter temperature
at 650°C, NOx

GAS BLENDER SETTINGS:

INSTRUMENT RESULTS

<u>Blend Gas (L/Min)</u>	<u>Dilution Gas (L/Min)</u>	<u>Blended Value</u>	<u>Instrument Value</u>	<u>% Deviation</u>
0.0	2.0	0	0	0.0
2.0	0.0	277	277	0.0
1.5	0.5	208	207	0.2
1.0	1.0	138	138	0.0
0.5	1.5	69	70	0.2
0.0	2.0	0	0	0.0
2.0	0.0	277	276	0.0

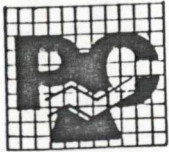




INSTRUMENT AND CALIBRATION DATA

<u>ANALYZER</u>	<u>RANGE</u>	<u>ZERO GAS</u>	<u>SPAN GAS</u>
<u>TYPE:</u> NO/NOx			
<u>MANUFACTURER:</u> Thermo Electron	0-500	Ambient Air	99.94 <u>1/</u>
<u>MODEL:</u> 10			
<u>SERIAL #:</u> 10 A/R-17380-169			
 <u>TYPE:</u> O ₂			
<u>MANUFACTURER:</u> Teledyne	0-25%	N ₂ <u>1/</u>	Ambient Air
<u>MODEL:</u> 320 AX			
<u>SERIAL #:</u> 90840			

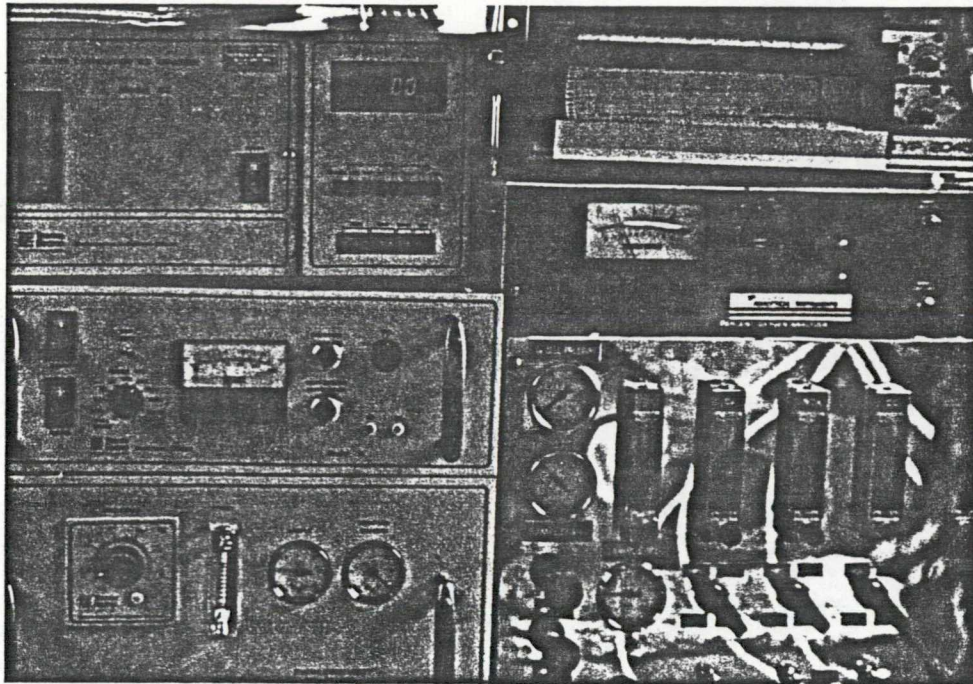
1/ Cylinder AAL-14186 (see certification data Appendix D)



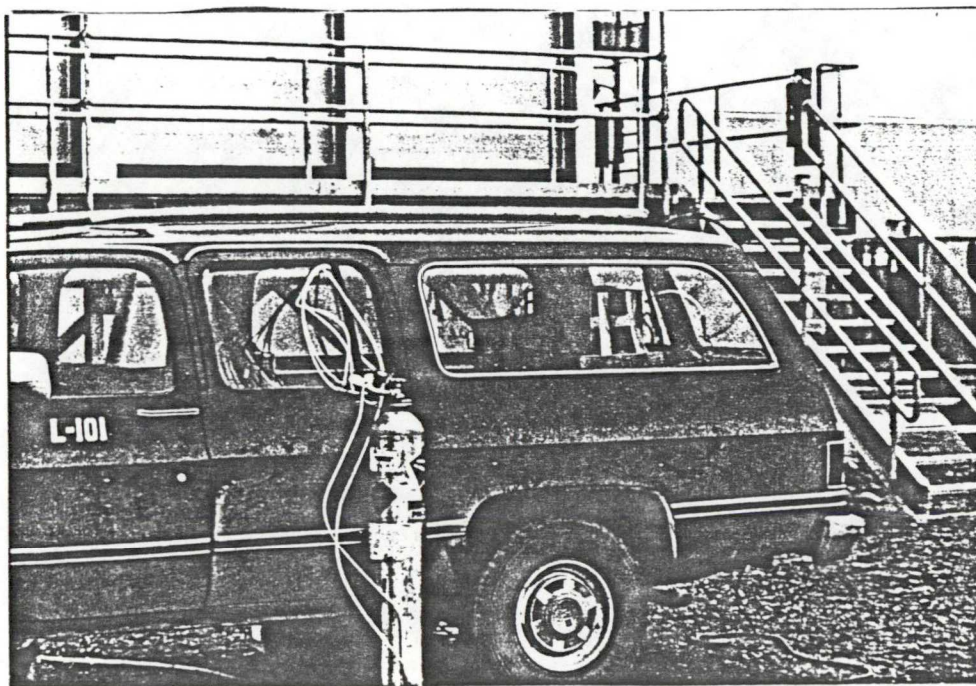
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APPENDIX E

SAMPLE SITE PHOTOS

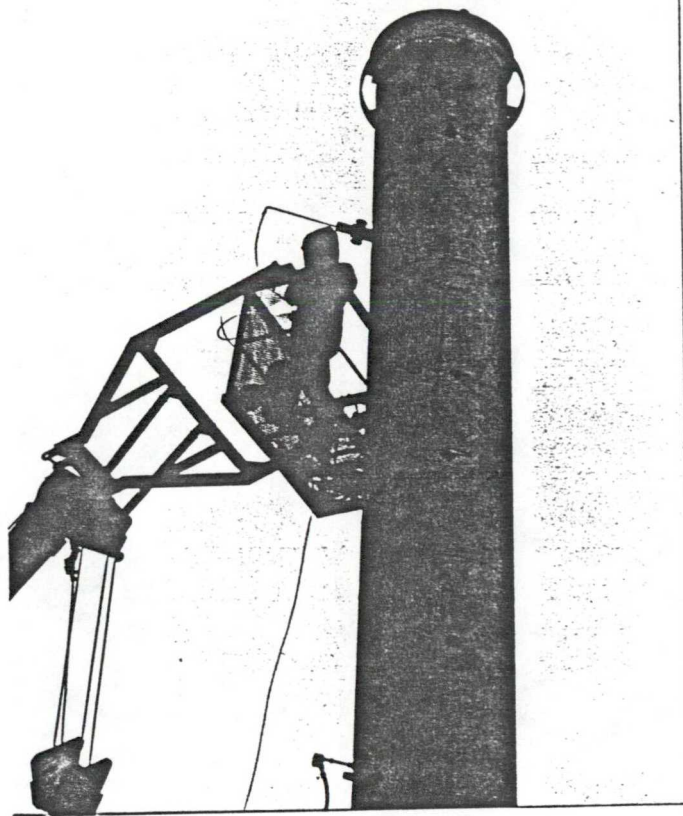


Instrument set-up

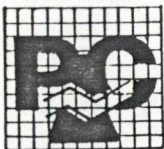


Instrument vehicle & calibration gases

KUPARUK UNIT TOPPING PLANT



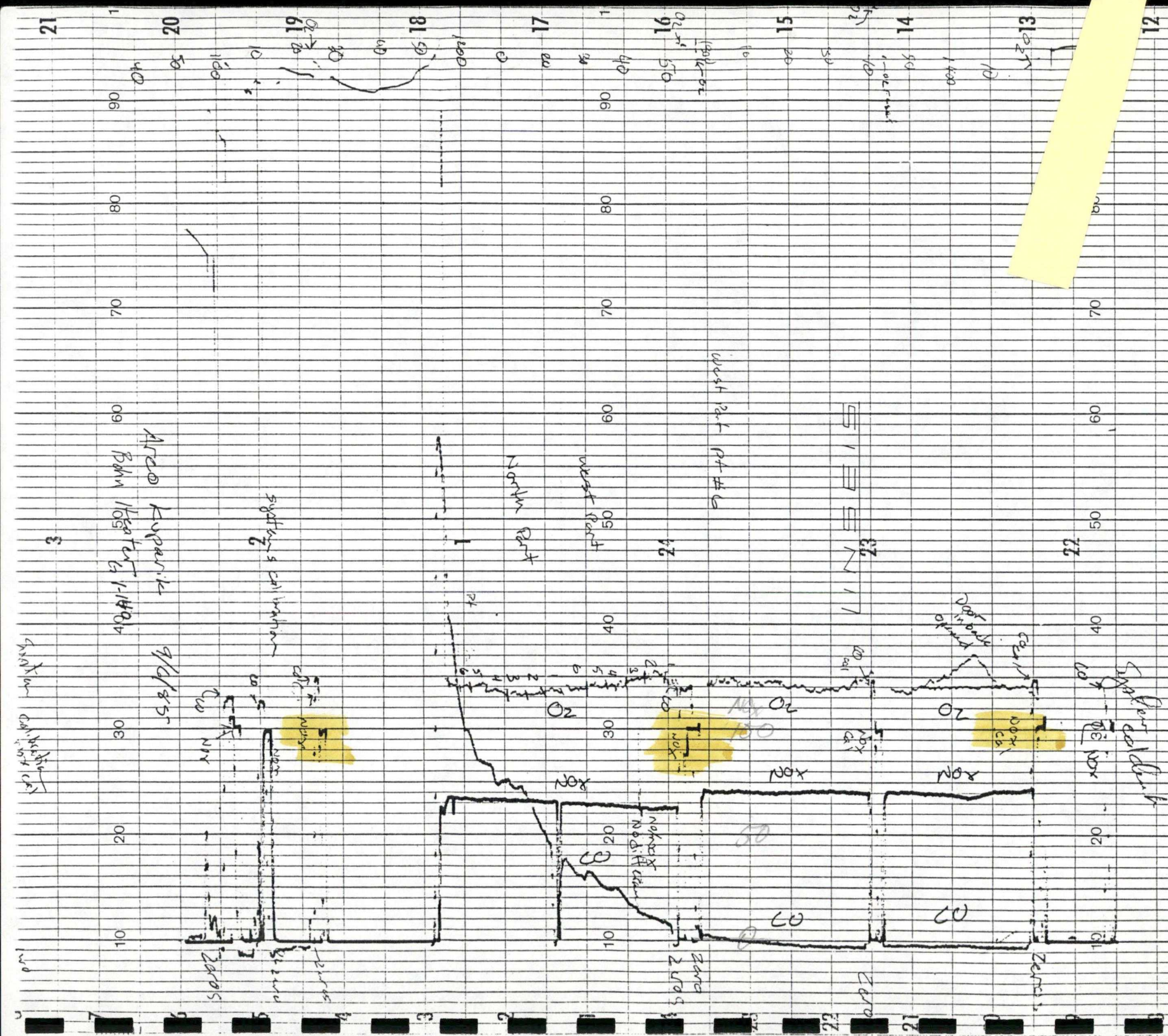
Bohn Inc. 44.44MMBtu/hr Heater

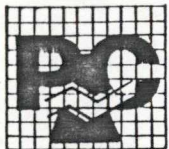


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APPENDIX F

STRIP CHARTS





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APPENDIX G

RELATED CORRESPONDENCE



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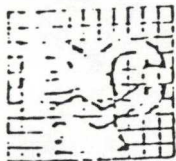
SOURCE TEST PLAN

- I. Client: Kuparuk River Unit Owners Represented By:
ARCO ALASKA INCORPORATED
P.O. Box 100360
Anchorage, Alaska 99510

Attention: Jim Ives (907) 263-4307
- II. Testing Firm: Petro-Chem Environmental Services
3207 Antonino Avenue
P. O. Box 5126

Attention: Leslie Johnson
(805) 327-7300
- III. Unit To Be Tested:
One (1) 44.44 MMBTU/hr. Bohn Heater
(Arco tag # G1-14-01). The unit will
be operating on gas for a fuel, with a
normal heat release approximately 35.56
MMBTU/hr.
- IV. Procedures:

Determination of NO_x, and O₂ concentrations and emissions
from the 44.44 MMBTU/hr heater located in Kuparuk River
Alaska. Monitoring of NO_x, and O₂ will be by continuous
monitoring analyzers (see attachment A) and documented with
an analog strip chart recorder. Three, forty minute test
runs will be conducted at each unit with zero and span
calibrations before and after each test. During each test
the units operation parameters will be monitored to
document its load capacity. An oxygen traverse will be per-
formed on all turbines and heaters to determine test run
sampling points. If upon completion of the oxygen traverse,
no deviation is found, single point sampling will be done
on the heater.



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Procedures Cont.

Volume flows and operating conditions of each unit will be calculated using the process conditions which are documented, and will be made available, by the process engineer. A gas sample will be taken for each unit and analyzed by ARCO's Laboratory. If the available information does not satisfy EPA Region X DEC, EPA Method 2, 3, and 4, will be performed to document volume flows.

The analyzers which are to be used for testing are:

Thermo-Electron, Model 10;
Chemiluminescent NO/NO_x Analyzer
Serial No: 10A-R-17380

Teledyne Instruments, Model 320-AX
Fuel Cell O₂ Analyzer
Serial No: 50840

Testing Dates:

September 6 or 7 1985

Attachment A

CONTINUOUS EMISSION MONITORING SYSTEM (CEMS)

Reference: BAAQMD, Manual of Procedures; ST-13A, St-19A, Jan 1982 State of California, Air Resources Board, Test Methods 1-100, June 1979 CRF 40 parts 53 to 80, Test Methods 7E and 20, 1985.

INSTRUMENTATION SUMMARY:

A constant sample of flue gas was extracted, dried, filtered, and delivered to an instrument manifold system for distribution to one or more analyzers. Instrument results are recorded on an analog strip chart recorder. System calibration checks are performed at the beginning and end of each day as well as calibration check at the beginning and end of each test run. Final data reduction includes zero and calibration drift corrections.

SAMPLE CONDITIONING SYSTEM:

Consists of a borosilicate glass tube or 316 grade stainless steel probe fitted with a cindered stainless steel or pyrex glass wool particulate filter. The probe is fitted with a teflon (TFE) sample line which connects to a water condensation system located at the sources. The condensation system consists of three 500 ml glass impingers connected in a series, immersed in an ice bath. The gas is delivered to the instrument van with a teflon line (3/8" O.D.) through an in line Balston particulate filter drawn by a teflon coated diaphragm pump. The sample system is leak checked prior to sampling by plugging the end of the sample probe and adjusting the sample pump to it's maximum rate (approximately 22" Hg). The manifold is bypassed and the leak rate monitored through a gas meter or low range flow meter.

MANIFOLD SYSTEM:

Sample gas is delivered to each analyzer through a five (5) way valve and regulated with a needle valve flowmeter. Manifold pressure is controlled by a back pressure regulator which is typically set at three (3) psi. Zero gas (N₂) and calibration gases are delivered to the analyzers using the same five-way valve and flowmeter. All manifold parts are glass, stainless steel, or teflon materials.

CALIBRATION PROCEDURES:

A. System Calibration Procedures:

System calibration checks are performed at the beginning and end of each test day to insure against sample system leaks or contamination. Calibration gas is introduced at the sample probe tip at a normal sample rate and vacuum, the final instrument value must be within $\pm 5\%$ of the calibration gas value.

B. Manifold Calibration:

Instrument calibration checks are performed and adjustments made before and after each test run. Each analyzer is checked with a zero grade nitrogen gas for a zero baseline and then with a calibration gas similar to the expected sample concentration (60-90% of full scale). Calibration gases used in both manifold and system calibrations are with EPA protocol No. 1 gas (traceable to National Bureau of Standards SRM,) or with gases recently analyzed by EPA Reference Methods. All zero and calibration checks are documented and noted on the recorder strip charts.

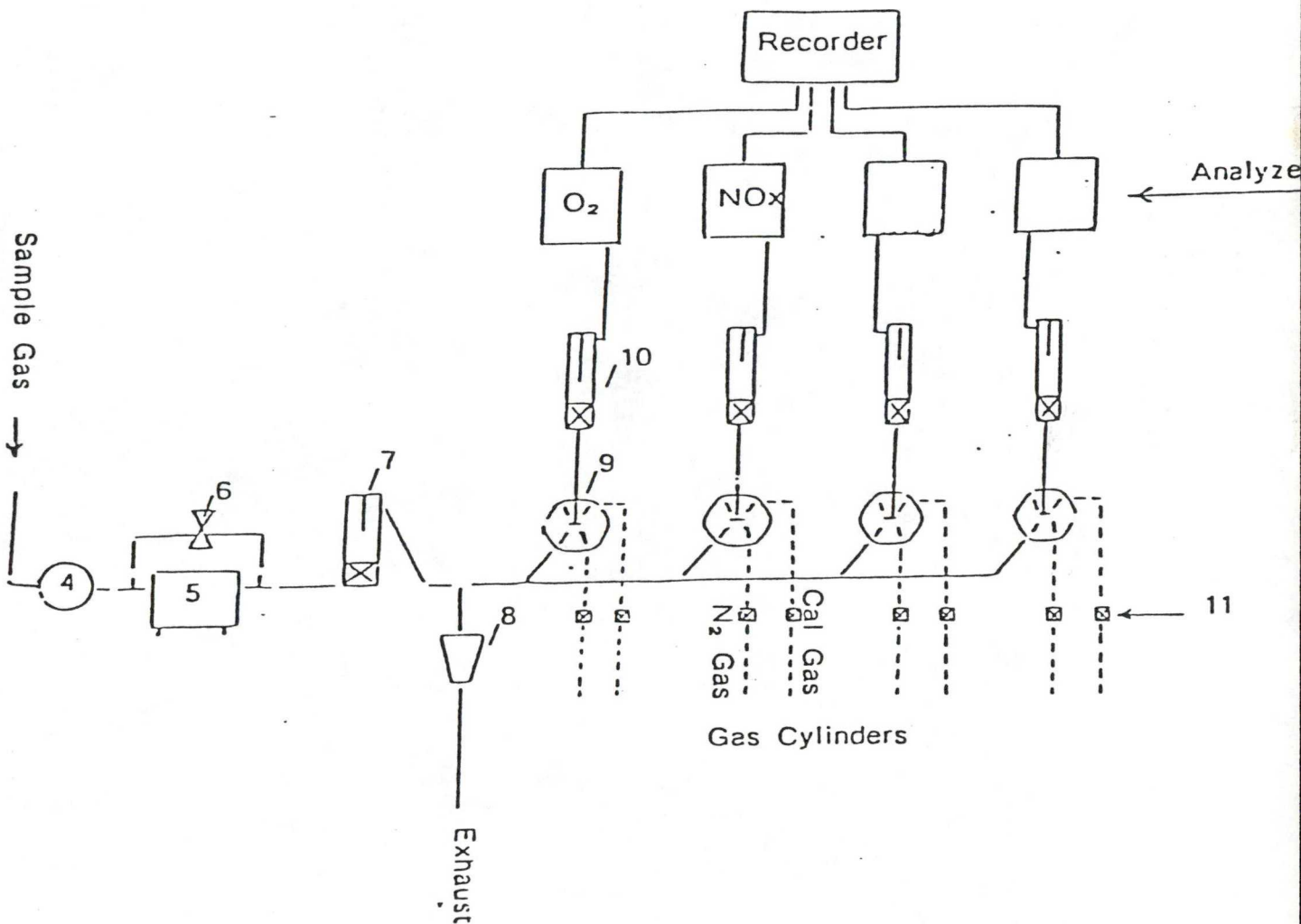
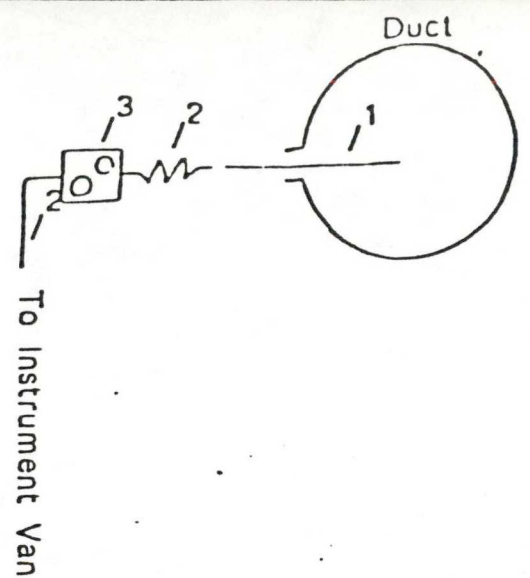
Not
Method
20

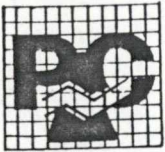
ANALOG STRIP CHART DATA REDUCTION:

Analog recordings were averaged of time increments as shown on the data pages (typically 5, 10, or 20 minute increments). Data for each increment was recorded at an average percent of full scale. The readings were then compared with the zero and calibration readings for calculation of the average concentration for each time increment. Any deviation of the zero and calibration readings from the start to the end of a test period was corrected by calculating apparent zero and calibration readings for the mid-point of each time increment. The average concentrations were then calculated from the sample readings and the apparent zero and span readings.

PNEUMATIC DIAGRAM

- 1) 316 Stainless Steel Probe
- 2) Teflon Sample Line
- 3) Sample Gas Conditioner
- 4) Filter
- 5) Teflon Coated Diaphragm Pump
- 6) By-Pass Control Valve
- 7) Sample Flowmeter
- 8) Back-Pressure Regulator
- 9) 5-Way Gas Selection Valve
- 10) Instrument Flowmeter
- 11) Metering Valves





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APPENDIX H

RESUME OF QUALIFICATIONS

EDUCATION:

1974-1978

California Polytechnic State University
San Luis Obispo, CA
School of Natural Resource Management
B.S. Environmental Science/Natural Resource Management

WORK EXPERIENCE:

August 1980 to December 1984

Chemecology Corporation
18823 Porterville Highway
Bakersfield, CA 93308

January 1985 to Present

Petro-Chem Environmental Services
3207 Antonino Avenue
Bakersfield, CA 93308

JOB CLASSIFICATION:

Project Supervisor/Air Quality Consultant/Division Manager

Job Description: Ms. Johnson has had extensive experience in field source testing, technical report writing and administrative organization of a source testing company. She has compiled approximately 250 technical reports for both engineering and compliance testing for EPA regions IX and X, CARB, Kern County APCD, South Coast AQMD, Bay Area APCD, and other California Agencies.

The job requirements include bidding, test supervision, and report compilation while maintaining an intimate contact with the client and regulatory agency. In order to insure proper testing methodology and report documentation. Ms. Johnson's out-of-state testing experience includes Prudoe Bay-Alaska, Hawaii, and the Netherlands.

Specific areas of expertise include EPA reference methods 1-8, continuous instrument sampling, analytical chemistry, personnel training and business management.

EDUCATION:

1974-1976

Bakersfield Junior College
Bakersfield, California
Concentration: General Education

1977-1980

Chico State University
Chico, California
School of Agriculture
B.S. Agriculture
Concentration: Range Management, Plant &
Soil Science

WORK EXPERIENCE:

August 1980 to January 1985

Chemecology Corporation of Bakersfield
18823 Porterville Highway
Bakersfield, CA 93308

January 1985 to Present

Petro-Chem Environmental Services
3207 Antonino Avenue
Bakersfield, CA 93308

JOB CLASSIFICATION:

Source Test Team Leader/Air Quality Specialist

Job Responsibilities- Supervision of test teams during both compliance and engineering testing. Mr. Winkler has worked closely with clients from initial contact to the review of final reports. Since 1980 he has compiled and written approximately 150 reports for such agencies as: Environmental Protection Agency - Region IX and X, Kern County APCD, Monterey Bay Unified APCD, Fresno County APCD, Santa Barbara County APCD, and South Coast APCD.

Specific areas of expertise include: Extensive testing with continuous instruments, EPA reference method source sampling, analytical chemistry, equipment calibration and personnel training in continuous instruments, instrument manifold fabrication, and field sampling techniques. Some of Mr. Winkler's testing areas include Coopers Engineering-Germany, Sun Production, Texaco Inc., and extensive testing in the Prudoe Bay Area for both Sohio Alaska and Arco Alaska Companies.